

Optimizing CO₂-mixture based power cycles for CSP applications: A multi-objective approach

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DESOLINATION Concept

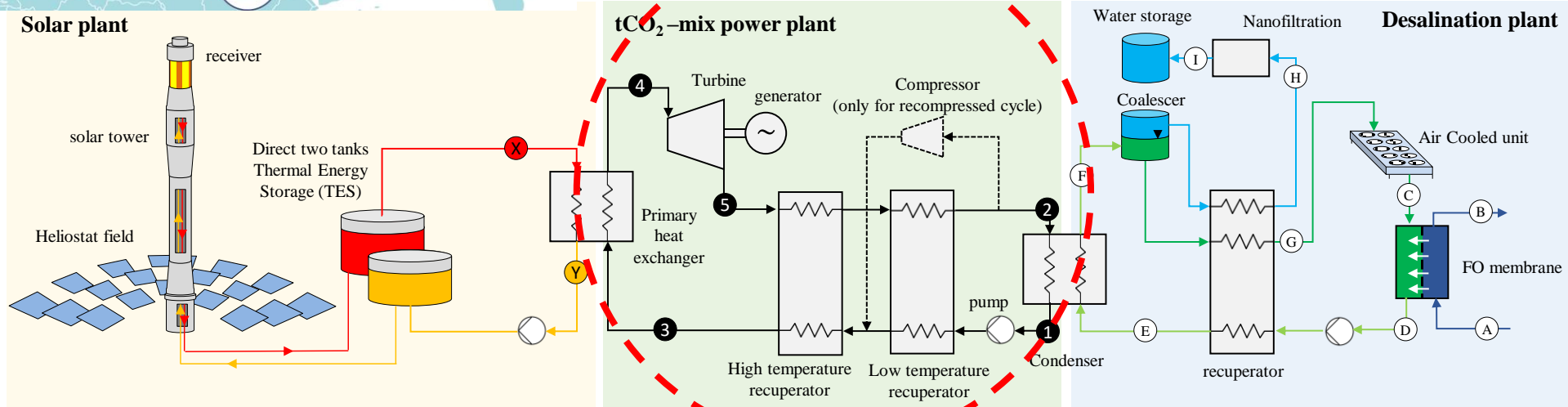


- 13 Universities
- 3 Research centre
- 2 Large Industrial Partners
- 4 SME

Duration: 64 months




Start Date: 01 Jun 2021

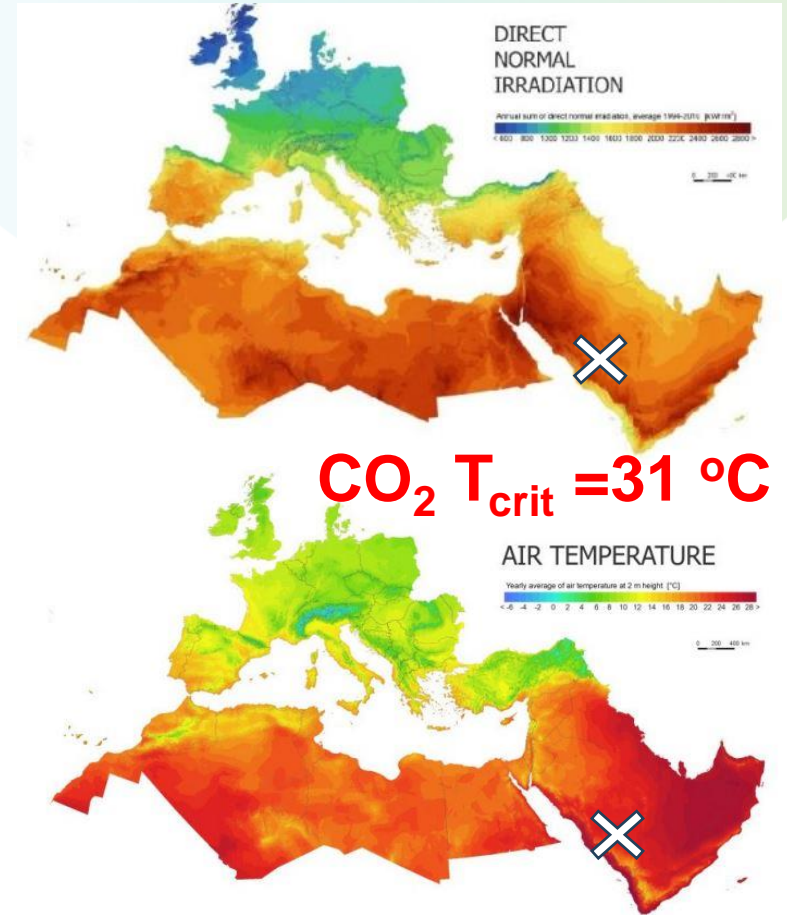
Estimated Project Cost: €13.8 mil



Research Gap

$$T_{\max} = 550/700^{\circ}\text{C} \quad T_{\min} = 50^{\circ}\text{C}$$

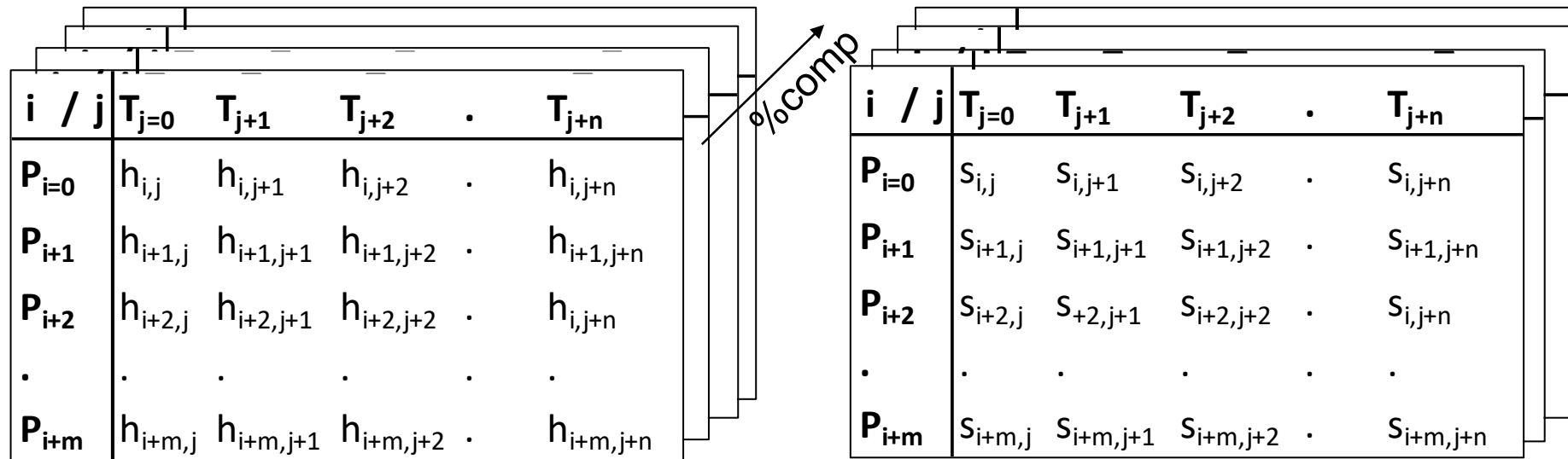
Generation	1 st gen.	2 nd gen.	3 rd gen.
Receiver outlet temp.	~250 - 450 °C	~500 - 565 °C ~720 °C	Expected to be >700 °C
Typical plant or technology	PTC, SPT, LFR 	PTC, SPT, LFR, PDC ~500 - 565 °C 	Salt, Particle, Gas 
Heat transfer medium	Oil or steam	Steam or salt	Salt, Particle, Gas
Thermal energy storage	Early designs: No or small Recent designs: Yes	Early designs: No or small Recent designs: Yes	No Yes
Power cycle	Steam Rankine cycle	Stirling	Brayton cycle
Peak temp. of cycle	~240-440 °C	~480-550 °C ~720 °C	Expected to be >700 °C
Design cycle eff.	~ 28-38%	~ 38-44% ~38%	Expected to be >50%
Annual solar-electric eff.	~ 9-16%	~ 10-20%	~ 25-30%



Khan et al. 2022. Progress in technology advancements for next generation concentrated solar power using solid particle receivers

Dopants and properties

	CO ₂ +C ₆ F ₆	CO ₂ + SO ₂	CO ₂ +SiCl ₄	CO ₂ +TiCl ₄	CO ₂ + C ₂ H ₃ N
BIP	0.033	0.0242	0.13933	0.0745	0.054
EoS	Standard PR	Standard PR	Standard PR	Standard PR	Standard PR
Thermal levels	550°C Only	550 and 700°C	550 and 700°C	550 and 700°C	550°C Only

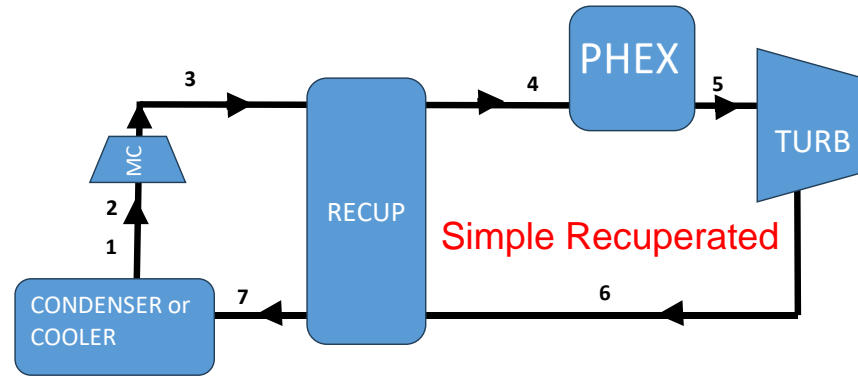


Resolution

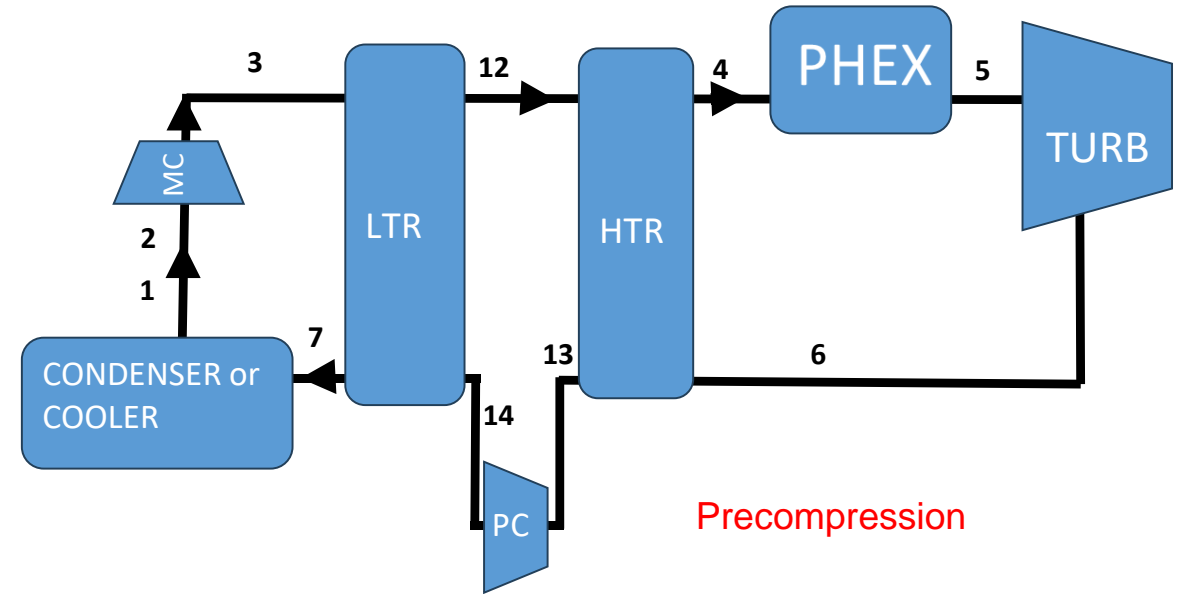
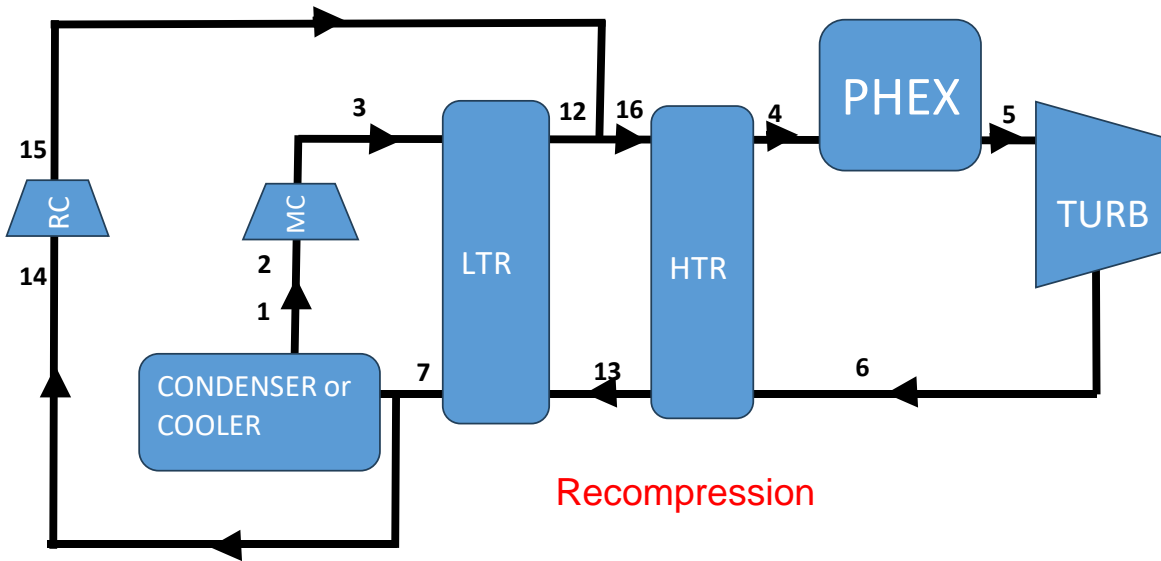
- 1°C (390-750)
- 1 bar (20-300)
- 1% (50-100)

Chemical Engineering Design Library (ChEDL)
<https://github.com/CalebBell/thermo>

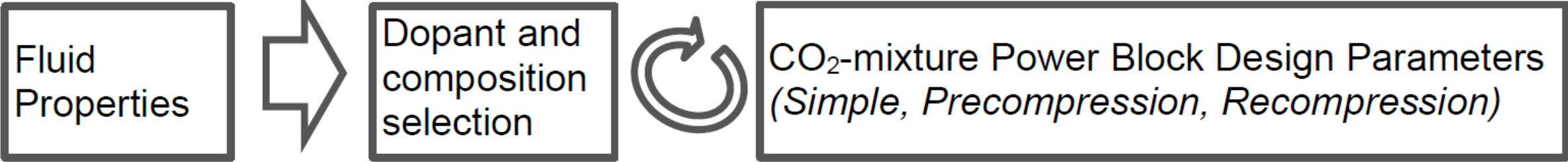
Cycle Layouts



Isentropic efficiencies
Minimum pinch for HEXs
Pressure drops accross HEXs

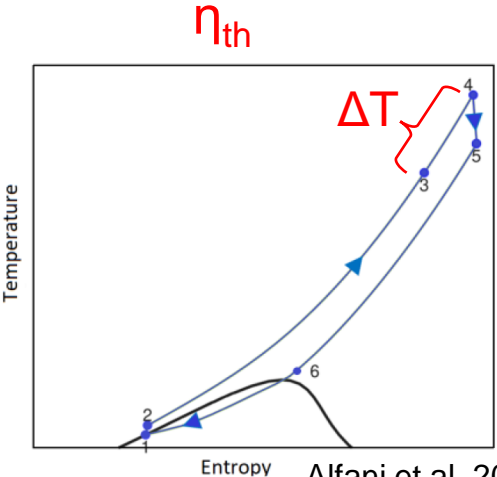


Simultaneous Optimisation Strategy



Proposed simultaneous Multi-objective Global Optimization with MATLAB

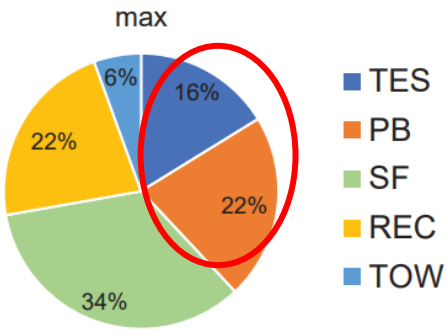
Thermal efficiency vs ΔT across PHEX \rightarrow Multi-criteria decision-making



Max η_{th} \rightarrow Min Solar Field cost

Max ΔT \rightarrow Min TES Costs

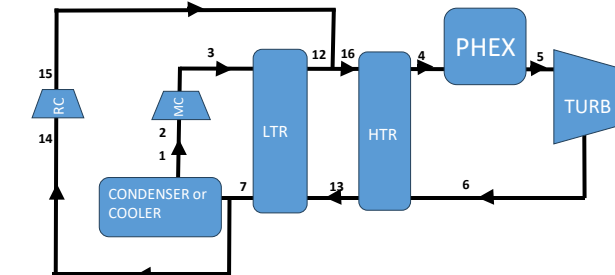
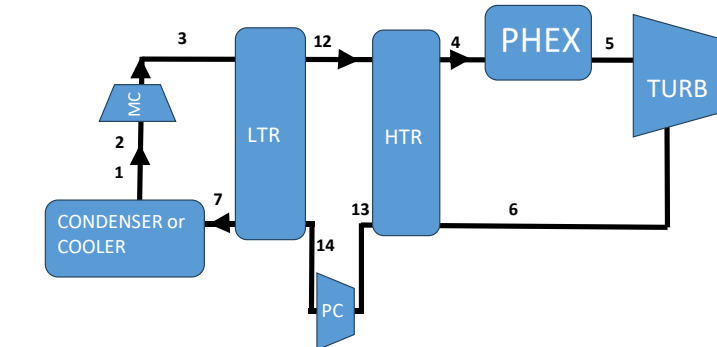
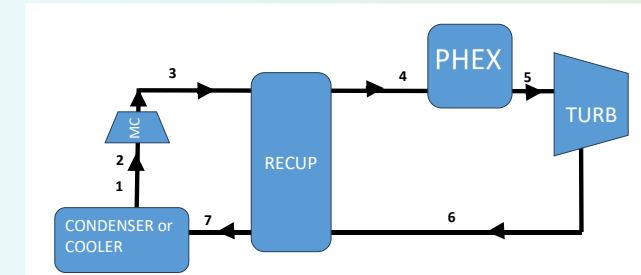
Max spec work \rightarrow Min Power Block cost



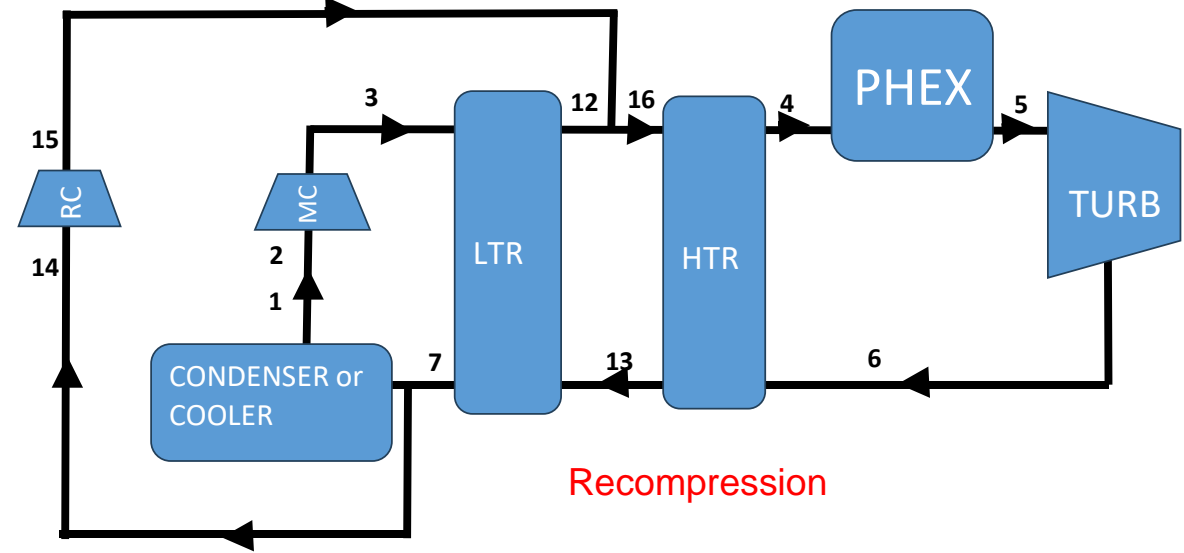
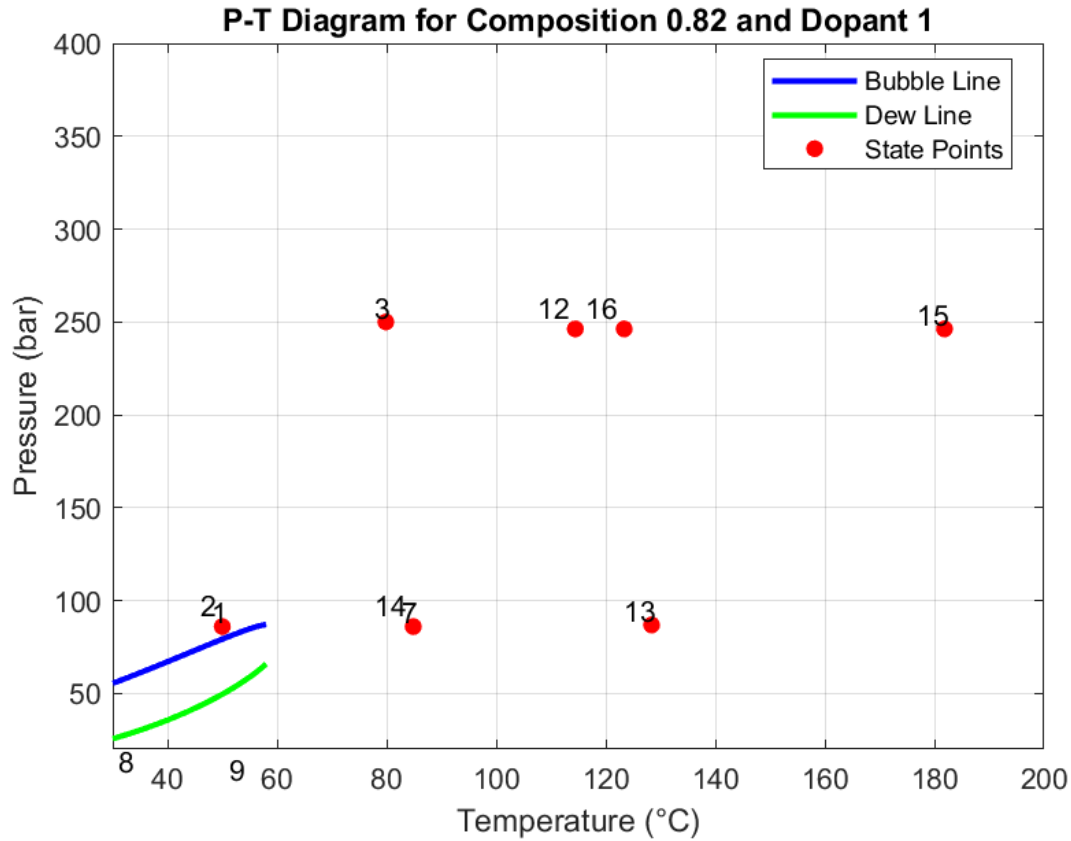
Alfani et al. 2022. Techno-economic analysis of CSP incorporating sCO2 brayton power cycles: Trade-off between cost and performance

Boundary Conditions and Bounds

	T_{max}	Dopants	CO ₂ Composition	T_{min}	P_{min}	P_{max}	PR	Split Ratio
Simple Recuperated	550°C	SO ₂ TiCl ₄ SiCl ₄ C ₂ H ₃ N C ₆ F ₆	50% to 100%	50°C	60 to 140 bar	250 bar	-	-
	700°C	SO ₂ TiCl ₄ SiCl ₄						
Precompression	550°C	SO ₂ TiCl ₄ SiCl ₄ C ₂ H ₃ N C ₆ F ₆	50% to 100%	50°C	40 to 120 bar	250 bar	1 to 2	-
	700°C	SO ₂ TiCl ₄ SiCl ₄						
Recompression	550°C	SO ₂ TiCl ₄ SiCl ₄ C ₂ H ₃ N C ₆ F ₆	50% to 100%	50°C	60 to 140 bar	250 bar	-	0 to 1
	700°C	SO ₂ TiCl ₄ SiCl ₄						

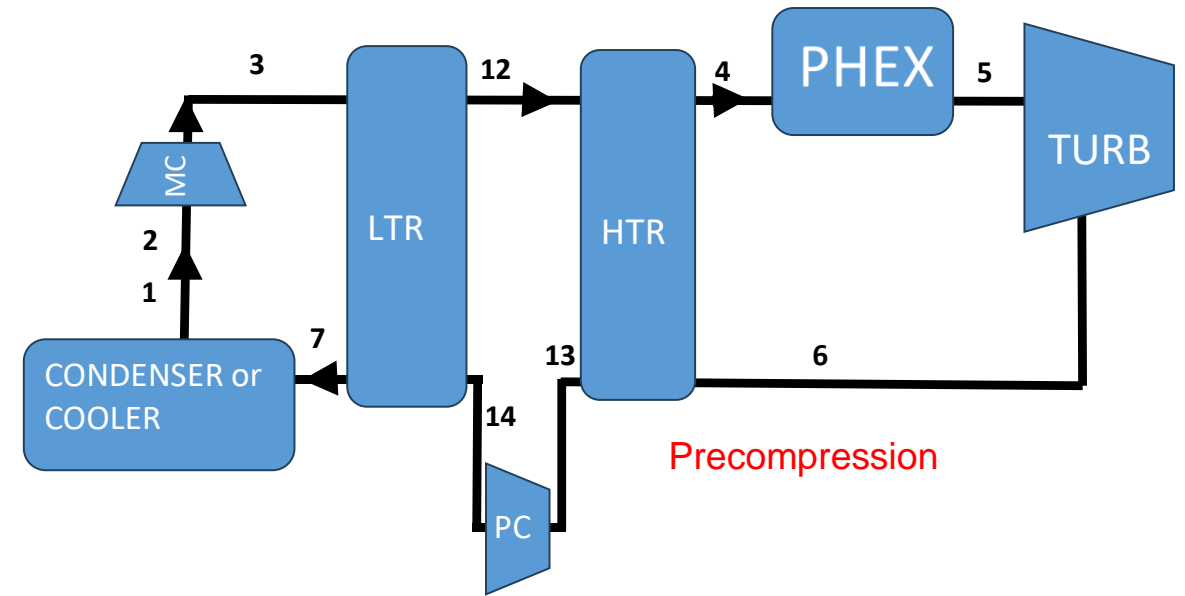
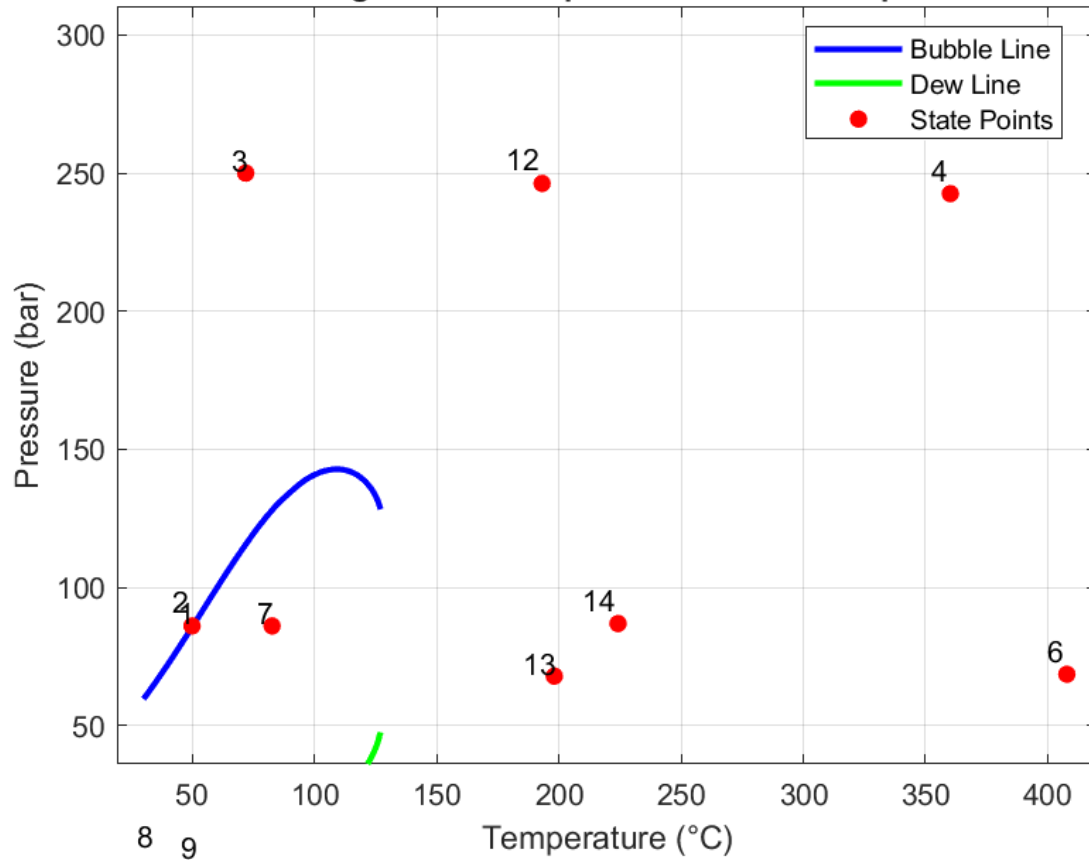


Constraints for termination



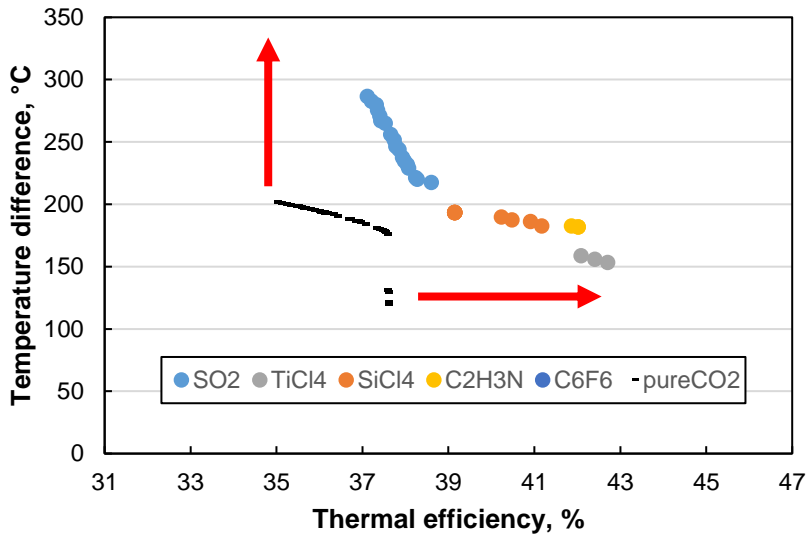
Constraints for termination

P-T Diagram for Composition 0.87 and Dopant 4

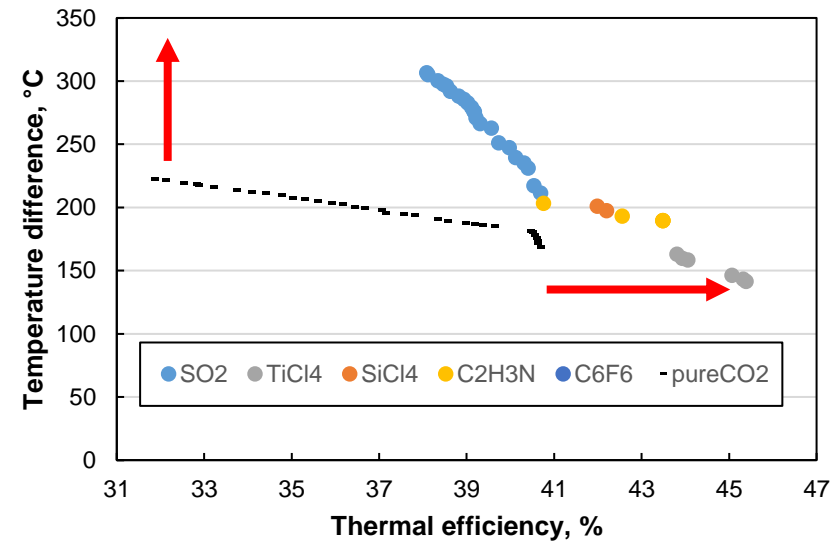


Genetic Optimization Results

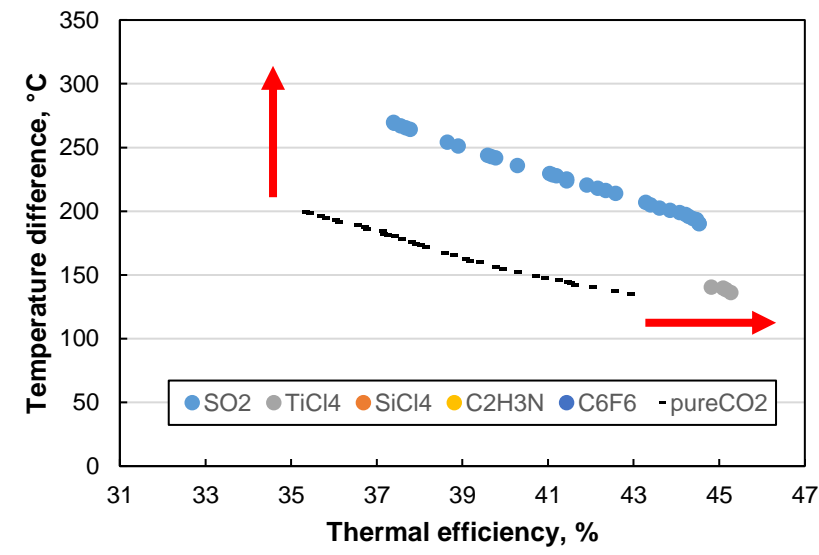
550 °C



Simple Recuperated



Precompression



Recompression

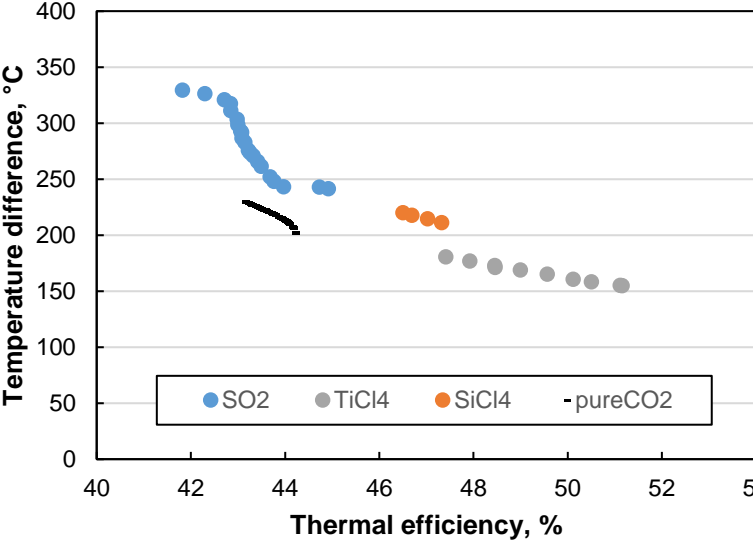
mcdm



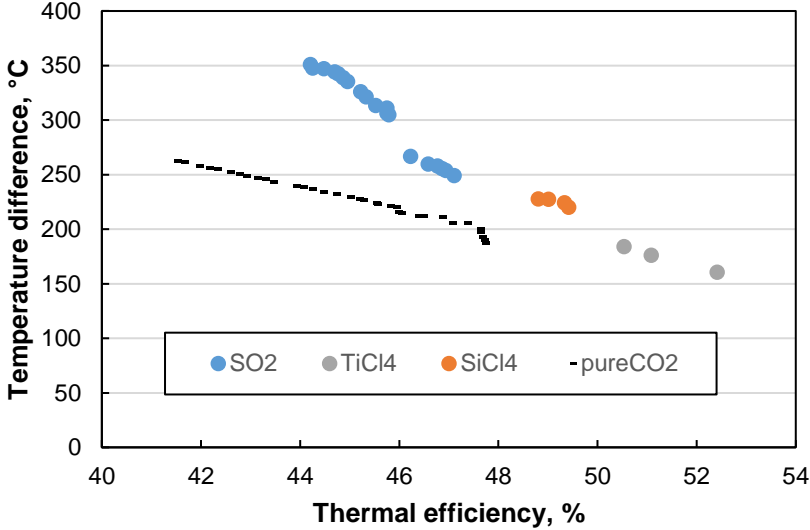
DESOLINATION

Genetic Optimization Results

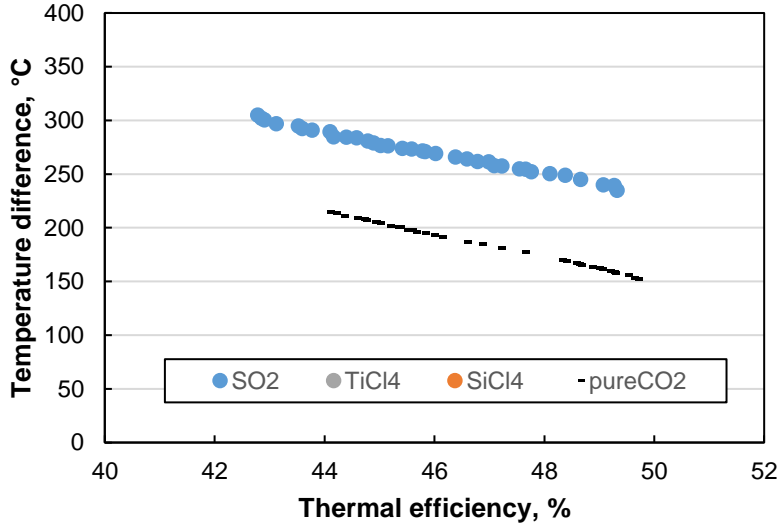
700 °C



Simple Recuperated



Precompression



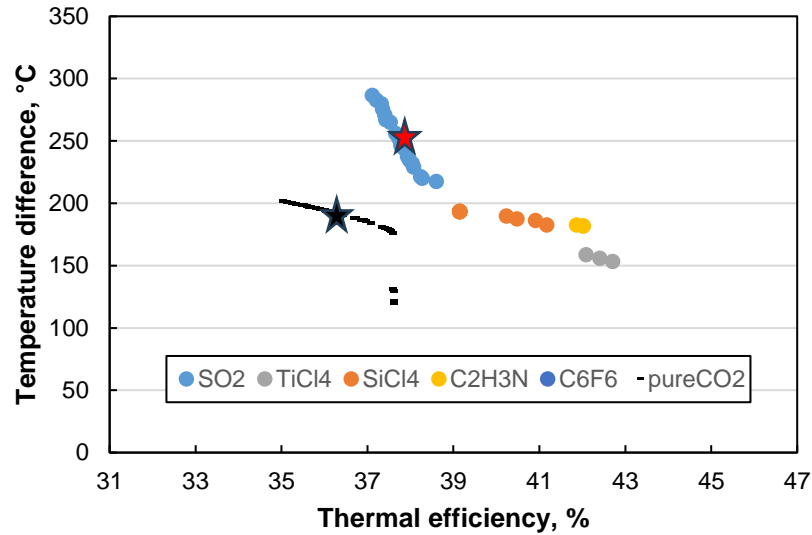
Recompression



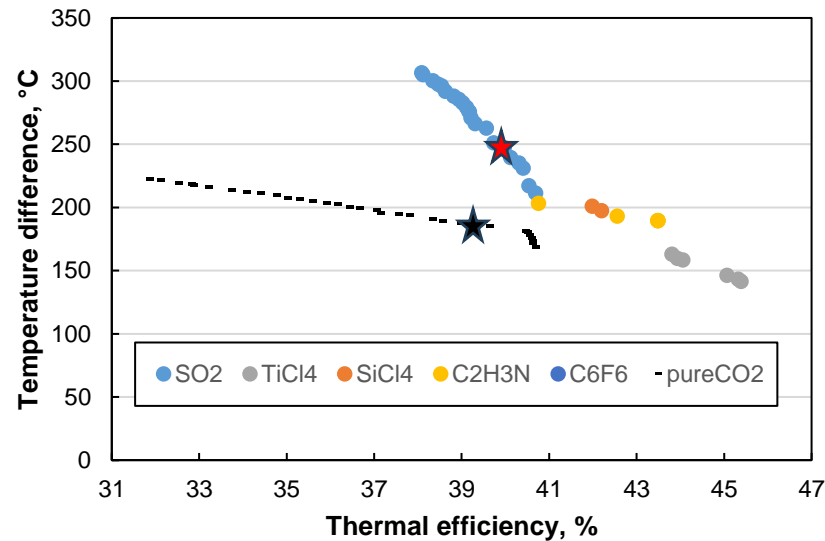
Multi-criteria Decision Making (MCDM)

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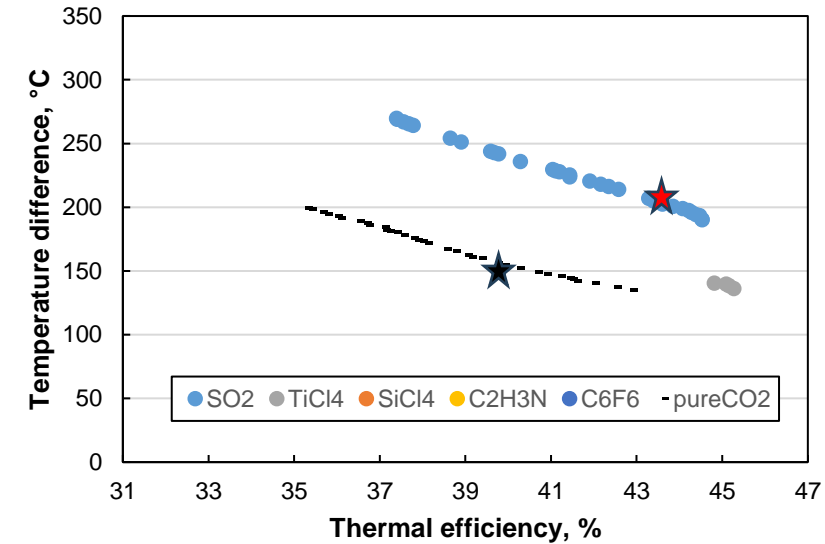
550 °C



Simple Recuperated



Precompression



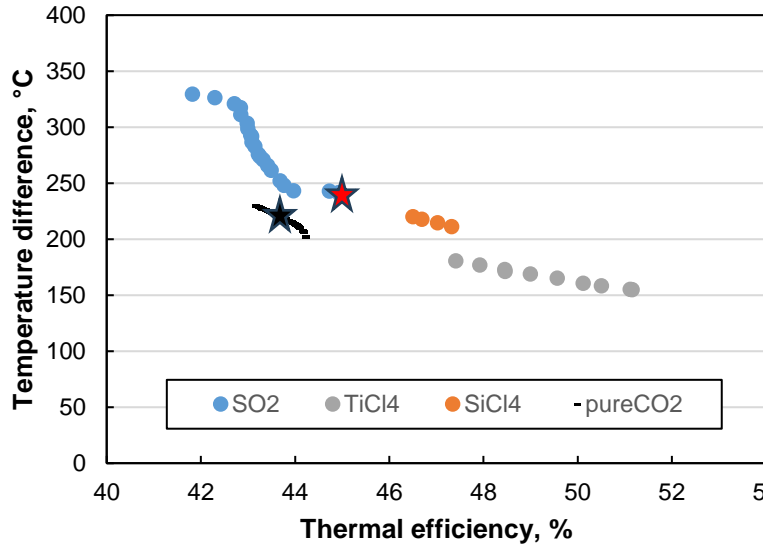
Recompression

Standard weightage: 50% η – 50% ΔT

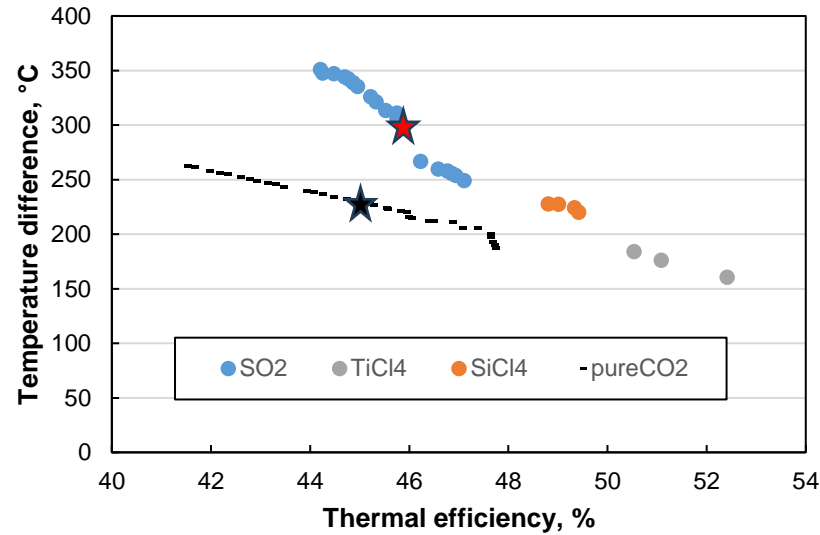
Method: TOPSIS L_∞

Multi-criteria Decision Making (MCDM)

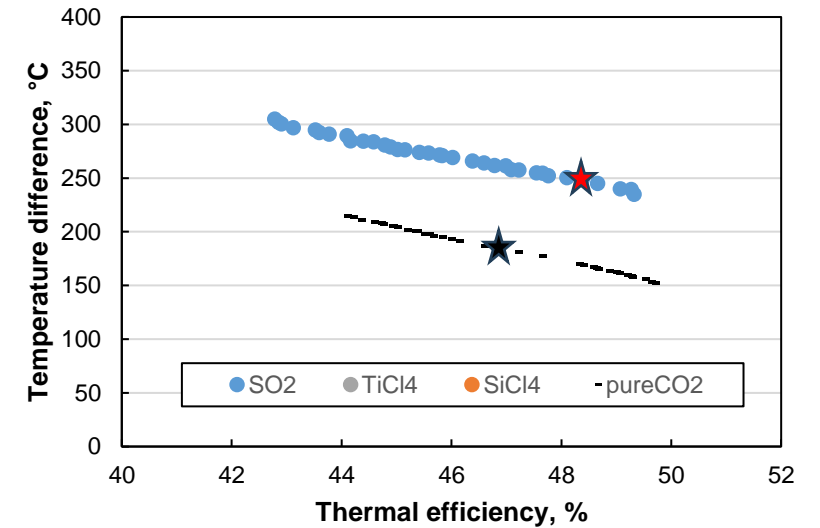
700 °C



Simple Recuperated



Precompression



Recompression

Selected solutions and improvements

Blend cycles

	T_{max}	Dopant	Molar CO ₂	P_{min} (bar)	PR	Split Ratio	η_{th}	ΔT	ω (kJ/kg)	capex (\$/kWe)
Simple	550°C	SO ₂	82.0%	79.3	-	-	38.0%	231.9	106.9	522.2
Recuperated	700°C	SO ₂	85.0%	71.3	-	-	44.9%	241.4	131.1	581.4
Precompression	550°C	SO ₂	77.6%	59.9	1.45	-	40.4%	231.0	111.4	624.6
	700°C	SO ₂	71.9%	63.0	1.39	-	46.6%	259.6	139.9	670.9
Recompression	550°C	SO ₂	67.4%	66.7	-	39.7%	44.2%	197.4	102.0	613.0
	700°C	SO ₂	66.7%	66.2	-	29.6%	48.3%	248.2	138.0	646.0

$\delta\eta_{th}$	% ΔT	% ω	%PBcapex
4%	23%	24%	-16%
3%	8%	7%	-14%
2%	24%	22%	-6%
3%	14%	8%	-7%
12%	23%	28%	-10%
4%	36%	4%	-13%

sCO₂ cycles

	T_{max}	Dopant	Molar CO ₂	P_{min} (bar)	PR	Split Ratio	η_{th}	ΔT	ω (kJ/kg)	capex (\$/kWe)
Simple	550°C	SO ₂	100.0%	74.0	-	-	36.6%	188.5	86.2	624.7
Recuperated	700°C	SO ₂	100.0%	64.1	-	-	43.4%	223.4	122.4	672.9
Precompression	550°C	SO ₂	100.0%	72.1	1.26	-	39.6%	185.6	91.6	663.3
	700°C	SO ₂	100.0%	55.1	1.22	-	45.2%	227.0	129.2	721.4
Recompression	550°C	SO ₂	100.0%	93.0	-	20.0%	39.3%	161.0	80.0	679.0
	700°C	SO ₂	100.0%	93.0	-	13.2%	46.5%	183.0	132.2	740.0

Conclusions

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- A list of dopants (5) can be explored for techno-economic performance for predefined layouts, t/c (3)
- Automated optimisation per layout with realistic conditions
- Multi-criteria Decision Making (MCDM) for two competing objectives, TES/HTF agnostic
- CO₂-SO₂ mixture dominating all temperature levels and cycle layouts
- ~20% decrease in PB CAPEX & TES costs for same or more efficiency

Shortcomings:

- Material compatibility and operational challenges
- Uncertainties in cost estimations for power block components

Thank You For Your Attention

Any Questions?



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